# EVOLUTION OF CO<sub>2</sub> AS REFRIGERANT IN ICE RINK APPLICATIONS

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## ABSTRACT

The first ice rink system using carbon dioxide,  $CO_2$ , as secondary refrigerant was built in Austria 1999. It would take until 2010 in Canada until the next generation, using a trans-critical  $CO_2$  solution, was realized for the first time. That eventually the ice rink business moved to trans-critical  $CO_2$  systems was a very natural step considering the 1<sup>st</sup> generation systems using  $CO_2$  as secondary refrigerant, and the parallel development of trans-critical  $CO_2$  systems in supermarkets. Ice rinks and supermarkets are rather similar when it comes to cooling capacity and heat recovery requirements which implies that the system design and associated control could easily be carried over to the ice rink applications.  $CO_2$  as refrigerant in both direct and indirect ice rinks systems where proposed several times before it eventually happened in 2010. The reason why it took so long before the ice rink industry accepted these systems is probably because there were no customers ready to take the risk and the somewhat higher cost for installing them. The most recent  $CO_2$  ice rink systems have demonstrated that essentially any ice rink can be self-sufficient with heat and that the overall energy efficiency is taken to a new level due to the unique properties of  $CO_2$ . Today we see a rapid growth in the number of  $CO_2$  ice rink systems in Canada, the U.S. and Sweden, which is most likely just the beginning.

Keywords: Ice rink, Carbon dioxide, Trans-critical, Refrigeration, Heat recovery, Controls

## **1. INTRODUCTION**

We are most likely experiencing the beginning of a paradigm shift in the way ice rinks are refrigerated. After the first ice rink system using carbon dioxide,  $CO_2$ , as secondary refrigerant was built in 1999, it took until 2010 before the first ice rink using a trans-critical  $CO_2$  system was realized. In this paper the rationales behind using  $CO_2$  in ice rinks are demonstrated together with the most important steps of the evolution of the technology. The latest generations  $CO_2$  ice rink systems have demonstrated that with proper design essentially any ice rink can be self-sufficient with heat, Rogstam and Bolteau (2015). In general the overall energy efficiency is taken to a new level due to the unique properties of  $CO_2$ .

#### 1.1 History of ice rinks

The history and evolution of ice rinks is well documented by Martin (1997) where it is concluded that the first known ice rink was the "The Glaciarium" in London from 1876. Technically it is described that "Copper pipes were laid down, and through these, a mixture of glycerine and water was circulated after having been chilled by ether." Most modern ice rinks could be described similarly, although the fluids would be different. The fast growing popularity of ice hockey in the 1880s added to the public demand for construction of ice skating rinks. The first mechanically refrigerated ice rink in the U.S. was constructed in 1879 and installed in the Old Madison Square Garden.

## 2. REFRIGERANTS AND SYSTEM SOLUTIONS

In the early days of refrigeration history, which starts in the 19th century, only natural fluids were used, since they were the only ones available. In the beginning of the 20th century, chemical science learned how to create substances with more "suitable properties" such as R12 and R22. Today R22 is subject to phase out according to the Montreal Protocol but is still in use in many ice rinks throughout North America. Due to the current focus on environmental issues and sustainability the refrigeration industry has to return

to the natural alternatives. Among these only a few are suitable for refrigeration purposes and the following ones are normally considered; ammonia, hydrocarbons and  $CO_2$ . In the industrial refrigeration sector, to which ice rinks count, ammonia has been widely used for decades. In recent times we have seen a growing interest to use  $CO_2$  as refrigerant in many applications, especially in the commercial sector. Since a few years back this development has begun to enter the industrial sector as well which will have considerable implications for the business.

## 2.1 Carbon Dioxide in the Refrigeration Industry

The history of  $CO_2$  can be divided into two parts where the first part is very well described by Williams and Bodinus (1999) who explained how the systems evolved and developed during the 19th and 20th centuries. They concluded that for the first part the interest in  $CO_2$  as a refrigerant virtually disappeared in the 1950s.



Figure 1. An advertisement for CO<sub>2</sub> systems originating from the early 20th century

It would take until the end of the 1980s when the Norwegian Professor Gustav Lorentzen brought up the idea of using CO2 again – and initiated the second part of the CO2 history. He investigated how the CO2 technology could be used in different applications and published numerous articles. Lorentzen (1993) stated that "CO2 is as close to the ideal refrigerant as it is possible to come…". He covered many aspects of using CO2 in his publications, not the least how heat may be reclaimed as well as the associated control strategies in order to optimise the process.

## 2.2 Properties of Carbon dioxide

Carbon dioxide is a natural, non-flammable and non-toxic substance which offers technical advantages of great interest when compared to the other natural alternatives. The challenge with  $CO_2$  basically stems from the fact that it has a critical point at a temperature of about 31°C with a corresponding pressure of about 74 bar<sub>a</sub>. At conditions above the critical point the difference between liquid and vapour disappears, thus no condensation occurs. With proper design however,  $CO_2$  systems offer good efficiency and low cost in many applications.

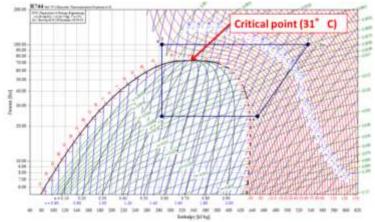


Figure 2. Schematic trans-critical CO<sub>2</sub> cycle in a p-h diagram.

## 2.3 Trans-critical solutions

This mode of operation is very relevant since most modern  $CO_2$  systems are designed to operate this way. The term trans-critical refers to the critical point as mentioned above. When the refrigeration cycle operates above and below the critical point, which is unique for  $CO_2$ , the mode of operation is called transcritical. This can be seen in Fig. 2.

#### 2.4 Commercial applications

Sawalha (2008) reports that the first Scandinavian installation of a trans-critical  $CO_2$  system took place in Denmark in 2003 and was followed by two Swedish installations in 2004. One of the pioneers in the transcritical  $CO_2$  supermarket area was Linde who presented the  $CO_2$  solution illustrated in the Fig. 3 below, Haaf et al. (2005). This system comprises a trans-critical supermarket  $CO_2$  systems including a heat reclaim function.

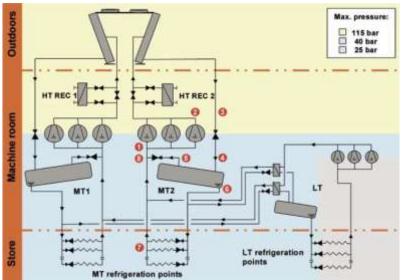


Figure 3. A schematic figure of a Linde trans-critical CO<sub>2</sub> system, Haaf et al. (2005).

#### 2.5 Heat reclaim

The concept of reclaiming heat from refrigeration systems is widely known and has throughout the history been implemented either "passively" by simply using the heat available, mostly de-superheat, or "actively" by controlling the head pressure to raise the temperature level of the rejected heat. The same principle applies to  $CO_2$  as well, with the only difference that there are some further implications as to the optimisation of the head pressure when operating above the critical point. This mode of operation and associated control was described by Lorentzen (1993) and further illustrated and applied by many others. In Fig. 4 Madsen (2010) illustrates the elevated head pressure in a winter case in order to reject the heat at a "higher" temperature.

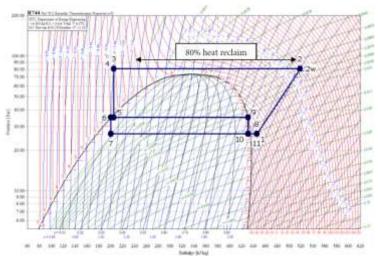


Figure 4. Illustration of the head pressure control to optimise the heat rejection based on the demand.

# **3. CO<sub>2</sub> ICE RINKS**

#### 3.1 First generation CO<sub>2</sub> ice rinks

Most ice rinks in the recent years have been built as indirect systems using a secondary refrigerant. There are a couple of secondary refrigerants commonly used in the industry which are listed below.

Name of substance	Abbreviation	Aqueous solution	Pure
Calcium Chloride	C.C.	Х	
Propylene Glycol	P.G.	X	
Ethylene Glycol	E.G.	X	
Carbon Dioxide, CO <sub>2</sub>	R744		Х

Table 1. Example of secondary refrigerants used in the ice rink refrigeration industry

Both propylene and ethylene glycol are relatively environmentally friendly but otherwise have rather poor properties, which results in high pumping power and thereby a lower overall performance of the refrigeration system. Calcium chloride which is a salt offers better efficiency in terms of pumping power than the glycols and is therefore still the most common solution, at least in European ice rinks. Calcium chloride however has practical challenges such as corrosion and is therefore phased out in favour of  $CO_2$  or ammonia-water.  $CO_2$  is used pure as a secondary refrigerant and from an energy perspective it offers significant advantages due to its low pumping power. Rogstam et al. (2005) compared  $CO_2$  to calcium chloride and concluded that  $CO_2$  requires less than 10% of the pumping power. On the other hand the system operating pressure is high so the rink floor piping system needs to be made of metal in order to withstand the pressure.

Ice rinks where  $CO_2$  is used as the secondary refrigerant in combination with a primary refrigerant are here referred to as "1st generation". The very first ice rink to be built with pump circulated  $CO_2$  as a secondary refrigerant and ammonia as primary refrigerant, was the Dornbirn ice rink in Austria 1999. Sulzer (Axima) designed and built the system, Axima (2005) as presented in Fig. 5.

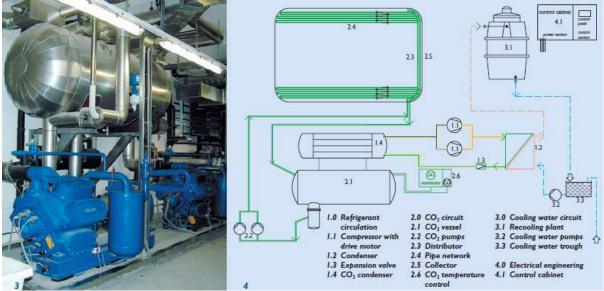


Figure 5. The ammonia- and CO<sub>2</sub>-based system in the 1999 Dornbirn ice rink, Axima (2004).

Axima and other companies in Austria, Germany, Switzerland, the Netherlands, Japan and Scandinavia continued using  $CO_2$  as secondary refrigerant in both new construction and retrofit after 1999. In 2015 there were 56 known ice sheets, in the world, cooled with  $CO_2$  as secondary refrigerant. A step forward in the development which reduced the installation cost was to use copper tubing in the rink floor. Rogstam et al. (2005) investigated this solution which resulted in the construction of the Backavallen ice rink in 2006. The compressors and the pump module of the Backavallen ice rink can be seen in figure 6. Another 15 rink floors have been built with this copper tubing technology from 2006 until 2015.



Figure 6. The Backavallen ice rink in Sweden with CO<sub>2</sub> as secondary refrigerant in copper tubes.

#### 3.2 Second generation CO<sub>2</sub> ice rinks – direct systems

In the light of what has been discussed so far, the use of  $CO_2$  as primary refrigerant in an ice rink application seems to be a very natural consequence. We normally refer to ice rink systems using  $CO_2$  as primary refrigerant as the "2<sup>nd</sup> generation". With the pump circulation  $CO_2$  systems evolving from the Dornbirn ice rink in 1999 and the parallel development of trans-critical  $CO_2$  system in the commercial sector, it became obvious to combine the two. In the early 2000s the components for trans-critical  $CO_2$  systems were not yet at the point where they needed to be, for instance in terms of compressor cooling capacities. As a consequence a  $CO_2$  ice rink refrigeration system would have required about 15 compressors to meet the capacity needs, where a typically ammonia system would only use 2 compressors, which made the  $CO_2$  system seem expensive and impractical. This contributed to a relatively late introduction of the technology in ice rink applications although the potential advantages were known.

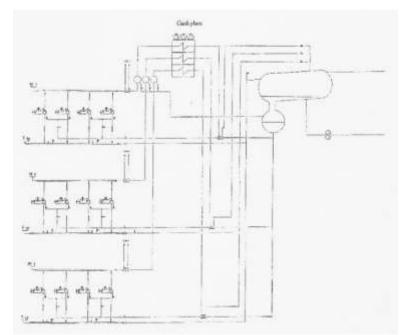


Figure 7. The proposed trans-critical CO<sub>2</sub> system in the Katrineholm city tender in January 2006.

The first known  $CO_2$  trans-critical ice rink design is the one that was proposed by Larsson (2006) for the Katrineholm city ice rink tender in January 2006. The proposed design for this tender, which can be seen in Fig. 7, illustrates the difficulties at the time in terms of the number of compressors. On the left in the figure the 12 compressors designed to meet the specified cooling capacity of 300 kW can be seen. The Katrineholm city eventually chose to install the prescribed 1<sup>st</sup> generation CO<sub>2</sub> system which was the first in Sweden at the time, so this proposed trans-critical CO<sub>2</sub> system was never built.

The second known trans-critical  $CO_2$  ice rink proposal is the 2009 Gentofte ice rink extension project in Denmark where one alternate tender consisted of a direct trans-critical  $CO_2$  system. The ice rink extension project was however postponed and eventually a traditional indirect ammonia solution was selected.

The first known direct  $2^{nd}$  generation CO<sub>2</sub> ice rink to be realised is the Arena Marcel Dutil in St Gedeon, Quebec, Canada in 2010. Due to being the first realized  $2^{nd}$  generation CO<sub>2</sub> ice rink, it has been well documented and Simard (2012) presented the system as can be seen in Fig. 8.

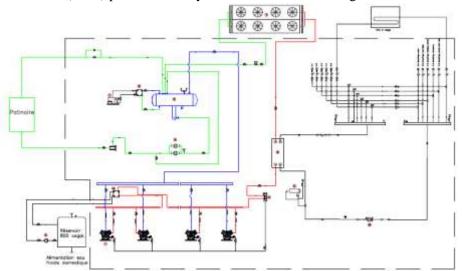


Figure 8. The trans-critical CO<sub>2</sub> system installed in St Gedeon 2010 (Simard 2012).

The system drawing shows the relationship and how the trans-critical  $CO_2$  supermarket systems have been combined with the 1<sup>st</sup> generation  $CO_2$  systems introduced in Europe. To the centre left, the liquid receiver is connected to the "green" circuit which essentially shows the pump circulation part of the system. Directly under the receiver, the liquid pumps are placed, which distribute the  $CO_2$  to the rink floor. In the bottom left part, 4 out of 7 compressors can be seen which are connected with the blue suction line to the liquid receiver. The red lines indicate the high pressure part from the compressor via the heat reclaim exchanger to the gas cooler. As reported by Simard (2012) a significant reduction of the energy cost was recorded which to a large extent can be explained by the heat reclaim. Further, the ice quality was recognised as being very good, which is a potential advantage with direct refrigeration of rink floors since they are typically easier to control.

#### 3.3 Second generation CO<sub>2</sub> ice rinks – indirect systems

 $CO_2$  can also be used as primary refrigerant in indirect ice rink systems where it cools a secondary refrigerant such as calcium chloride, glycols, etc. This solution is slightly less favourable from an energy standpoint, but it is still interesting in the case of a refrigeration system retrofit. The use of  $CO_2$  as primary refrigerant together with a secondary refrigerant in ice rinks has been proposed in the past, but it would take until 2012 before it was realized. First to publicly propose  $CO_2$  as primary refrigerant in ice rinks was IIHF (2002) and the second was a patent application from Mayekawa (2007). In Fig. 9 the transcritical  $CO_2$  system is indicated as the box 20 and the rink floor as number 4.

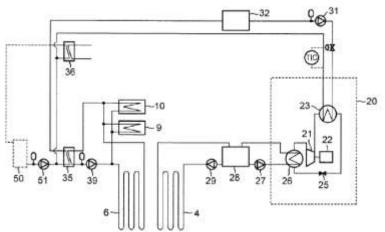


Figure 9. An indirect ice rink refrigeration system using  $CO_2$  as primary refrigerant with heat recovery. Still it would take until 2012 before the first indirect CO2 ice rink was built - the rewarded and wellrecognised installation at Dollar des Ormeaux, Quebec, Canada. This facility is an interesting example of

how the reclaimed heat from a CO2 ice rink system can be utilised to heat a swimming pool complex in addition to the ice rink itself. This installation is well described by Heon and Guerra (2015) and was awarded with the first price in the ASHRAE technology award case studies 2015.

# 4. DISCUSSION AND CONCLUSIONS

The basic system principle and functions of today's trans-critical  $CO_2$  ice rinks principally work exactly like the direct refrigeration systems from the past did, the difference is just the choice of refrigerant. As a matter of fact the very same system solutions and basic components apply regardless if the refrigerant is ammonia, R22 or even  $CO_2$ . For people in the refrigeration business it should be clear that  $CO_2$  has properties that are very suitable for ice rink applications, so we have to ask why it took so long until it was introduced, although it was identified as a potential solution several times in the history prior to 2010.

To find the answer we need to look back to the point where the natural refrigerant alternatives started their comeback. As described earlier, the revival of  $CO_2$  started with Professor Lorentzen's work and the first applications to be developed were automotive A/C systems in the early 1990s. In the beginning of this new  $CO_2$  era the components such as compressors etc., were developed and adapted for the rather small cooling capacities required in the automotive systems.

The next stage in the development was when the commercial sector began to adapt systems for  $CO_2$ , at the end of the 1990s. Primarily, the compressors were challenging to adapt for larger cooling capacities so the first supermarkets to be built had 10-20 compressors. The ice rink industry was however still used to normally work with 2 compressors. Using a large number of compressors would therefore inevitably affect the cost of the system in a negative way.

For  $CO_2$  to become a generally accepted system solution in the industrial sector all components had to be adapted in order to allow for practical designs such as higher allowed pressures, but not the least in order to lower the costs. Since the designs were new and the number of components manufactured was low, the price was often high. As the systems became more popular and the designs were further optimised the price decreased.

The compressor is a very vital component in the system as far as performance and cost are concerned. It is therefore a relevant example to illustrate the development in terms of the number of compressors required in order to maintain a single sheet ice rink. In the first trans-critical ice rink proposal from Larsson (2006), 12 compressors were required to meet the 300 kW cooling capacity requirement. When the Marcel Dutil Arena was built in 2010 it used 7 compressors which corresponded to a 317 kW of cooling. A recent  $CO_2$  ice rink project in Sweden uses 4 compressors to meet the specified cooling capacity of 250 kW, Rogstam and Bolteau (2015). These figures show the rapid development of the  $CO_2$  technology component-wise in the recent years.

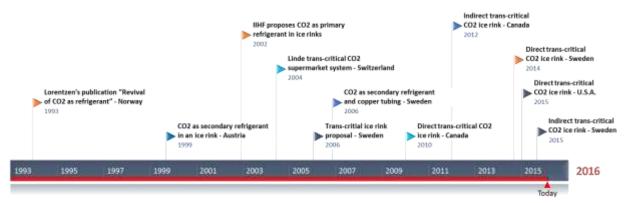


Figure 10. CO<sub>2</sub> ice rink technology evolution timeline.

The first ice rinks using  $CO_2$  as secondary refrigerant in Europe all used <sup>3</sup>/<sub>4</sub>" steel pipes in the rink floor. Three out of the first seven installed systems during 1999 and 2000 were "retrofits" which used existing pipe systems that previously carried ammonia. New systems with newly installed steel pipe systems were built as well, and between the years 1999 and 2004 about 23 ice sheets were built where half of them were new and the rest were retrofitted. The challenge with the steel pipe design was the cost of installation,

which indeed is the reason why the steel pipe design was abandoned in the 70ies in favour of plastic pipes. In order to use  $CO_2$ , however, there is no choice since the system pressure of  $CO_2$  requires metal pipes. Although a couple of ice rinks were built with  $CO_2$  from 1999 to 2004 the commercial success was not obvious.

The copper tube concept with  $CO_2$  as secondary refrigerant that was installed in the Swedish Backavallen ice rink proved to be a good technical solution, but it was still not enough to make a commercial success. The very same concept was installed in 5-6 new ice rinks in Sweden, Norway, Russia, Japan and Finland during the years 2005 to 2010 – still with  $CO_2$  used only as secondary refrigerant and in most cases in combination with ammonia.

In the beginning of the 2000s the so called trans-critical  $CO_2$  systems gained popularity and the first systems in commercial use were installed in 2003. With the introduction of the technology in the commercial sector, which had a significant cost focus, the cost of the system components decreased. Furthermore, it triggered the development of new and better adapted components that would allow for higher design pressures, make systems more practical and safer to handle and ultimately lead to more energy efficient solutions.

The reason why it took until 2010 before the ice rink industry accepted the 2nd generation systems is probably because there were no customers ready to take the risk and the somewhat higher cost for installing a trans-critical  $CO_2$  system. There was no demand for these systems but as the technology gradually became more refined in supermarkets, primarily in Europe but also in Canada, the confidence in the technology grew. The cost of components, and eventually the systems, decreased which opened the market for the 2nd generation  $CO_2$  ice rink refrigeration systems. Today we see a rapid growth in the number of  $CO_2$  ice rink systems in Canada, the U.S. and Sweden, which is most likely just the beginning.

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